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**PROBLEM 2.24** (continued)

$$\overline{Nu}_D = \frac{\bar{h}D}{k} = f(Re_D) \quad (c)$$

The Reynolds number is defined as

$$Re_D = \frac{V_\infty D}{\nu} \quad (d)$$

where

$V_\infty$  = free stream velocity, m/s

$\nu$  = kinematic viscosity, m<sup>2</sup>/s

Solving equation (c) for  $\bar{h}$

$$\bar{h} = \frac{k}{D} f(Re_D) \quad (e)$$

Applying (2) to the two spheres and taking the ratio to eliminate  $k$

$$\frac{\bar{h}_1}{\bar{h}_2} = \frac{D_2 f(Re_{D1})}{D_1 f(Re_{D2})} \quad (f)$$

where the subscripts 1 and 2 refer to sphere 1 and 2, respectively. Using (d) to determine the two Reynolds numbers

$$Re_{D1} = \frac{V_{\infty 1} D_1}{\nu} \quad (g)$$

and

$$Re_{D2} = \frac{V_{\infty 2} D_2}{\nu} \quad (h)$$

The total heat transfer rate is determined using Newton's law of cooling

$$q_T = \bar{h}A(T_s - T_\infty) \quad (i)$$

where  $A$  is surface area of sphere given by

$$A = \pi D^2 \quad (j)$$

(j) into (i)

$$q = \pi \bar{h} D (T_s - T_\infty) \quad (k)$$

Applying (k) to the two spheres and taking their ratio

$$\frac{q_1}{q_2} = \frac{\pi \bar{h}_1 D_1 (T_s - T_\infty)}{\pi \bar{h}_2 D_2 (T_s - T_\infty)} = \frac{\bar{h}_1 D_1}{\bar{h}_2 D_2} \quad (l)$$

**(iii) Computations.** Substituting numerical values in (g) and (h)

$$Re_{D1} = \frac{23.4(\text{m/s})3.2(\text{m})}{\nu(\text{m}^2/\text{s})} = \frac{74.88(\text{m}^2/\text{s})}{\nu(\text{m}^2/\text{s})}$$

and



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